

超临界压力下水冷壁中间集箱分配特性的研究

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摘要: 研究了国产600 MW 直流锅炉分配集箱水冷壁管在超临界压力下的流量分配特性。试验参数为: 压力 $p=23\sim 25$ MPa, 质量流速 $G=400\sim 1\,200$ kg/(m²·s), 工质温度 $t=10\sim 400$ °C。试验研究了工质压力、质量流速和工质温度对分配集箱垂直水冷壁管流量分配特性的影响。试验结果表明: 随着质量流速的增加, 垂直水冷壁管间流量分配的均匀性增加; 在拟临界点附近, 流量分配不均匀性有一阶跃增加, 而且随着压力的增加, 流量分配不均匀性在拟临界点的阶跃增加现象变弱。利用分配集箱并联支管的离散模型计算了分配集箱垂直水冷壁管内的流量分配, 计算结果与试验数据吻合。

关键词: 直流锅炉; 超临界压力; 分配集箱; 垂直水冷壁管

中图分类号: TK229.5 文献标识码: A

1 前言

由于超临界机组具有高效、安全、容量大和环境污染小的特点, 近年来我国电力行业正积极地开发和生产 600 MW 及以上的超临界变压运行直流锅炉。为了适应变压运行, 超临界锅炉的下辐射区一般采用螺旋管式水冷壁, 上辐射区为垂直管式水冷壁。垂直水冷壁管与螺旋管式水冷壁之间的连接多数是采用中间集箱, 即分配集箱, 通过分配集箱分配到垂直水冷壁管内的流量是否均匀直接影响超临界锅炉的安全运行。不少研究者对分配集箱内单相流体的分配特性进行了实验研究^[1~3], 但是这些研究一般局限在常压范围内, 对于超临界压力下分配集箱内流体的分配特性的研究未见报导。在超临界压力直流锅炉中, 分配集箱内的工质是单相水或单相水蒸气, 一般情况下不会发生严重的流量分配不均匀性, 但在大比热区 ($i=1\,700\sim 2\,500$ kJ/kg), 工质的温度变化时, 其物性发生显著的变化, 工质通过分配集箱后可能会引起水冷壁管流量有较大的偏差, 部分受热面蒸发管内流量变小, 就有可能发生工质

焓增加过多, 壁温过高而损坏的危险性, 直接影响着电站锅炉的安全运行。所以研究超临界锅炉在超临界压力下的流量分配特性具有重要的工程实际意义。

2 试验系统与试验参数

为模拟超临界锅炉水冷壁的实际工作条件, 试验在西安交通大学多相流国家重点实验室的高压汽水两相流试验台上进行, 试验回路系统如图1所示, 试验系统的详细说明可参考文献[6]。高压柱塞泵出口额定压力可达 32 MPa, 流量可达 4.5 t/h, 与试验回路上的阀门配合, 可保证试验系统的压力和流量调节到预定值。

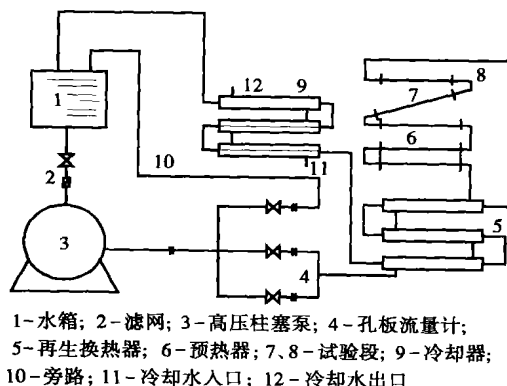


图1 试验系统回路简图

预热段采用交流电通过管子本身的电阻直接加热。为了减少散热损失, 换热器、预热段、试验段及其连接管路都用保温层进行了有效保温。

由于电加热功率的限制, 试验段采用了模型试验。因为影响分配集箱流量分配均匀性的主要因素

是工作压力、进口干度和质量流速,所以在试验段的工作压力、进口干度和某厂开发的 600 MW 超临界锅炉实际运行条件相同的情况下,在设计试验段具体尺寸时,保证试验段中集箱引入管的质量流速、集箱中质量流速和并联引出管内的质量流速与实际运行时的质量流速相等,从而使试验结果能反映实际运行情况。根据这一设计原则,确定出试验段的结构和尺寸如图 2 所示。从分配集箱进口开始沿分配集箱方向并联支管的编号依次为 1 号、2 号、3 号、4 号和 5 号支管;对应于实际集箱上的管子分别为 1 号、5 号、9 号、12 号和 16 号支管。

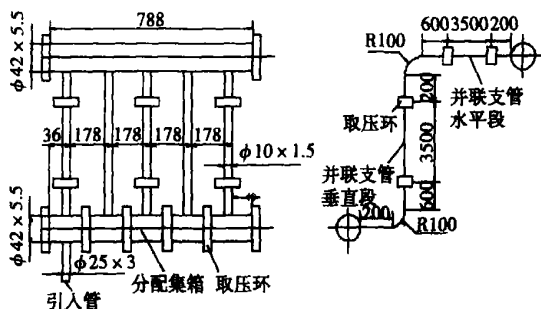


图 2 试验段结构及测点 布置图

为了对并联管束内的汽—液两相流进行双参数测量,并联管组设计成垂直管束和水平管束组合的方式,垂直管和水平管取压环之间的距离皆为 3.5 m,在试验段进口装有 Rosemount 3051 型压力变送器以确定压力;采用 115IHP 电容式差压变送器配合锐边孔板来测量试验段流量;电加热功率用测量到的电压和电流的有效值计算得到;垂直管和水平管取压环室之间的压差用 Rosemount 3051 型差压变送器测量。用 7 支 $\Phi 3$ 的 NiCr—NiSi 铠装热电偶测量系统工质温度,其中 6 支布置在预热段,1 支布置在试验段的进口。

本试验参数范围是:压力 $P=23、25$ MPa,分配集箱入口质量流速 $G=400 \sim 1\,200$ kg/(m²·s),介质温度 $t=10 \sim 400$ °C。

3 理论分析

为了更好地模拟实际流动情况,采用离散模型分析并联管组的流量分配^[7]。

3.1 分配集箱中支管部分的动量方程

对于第 i 根支管的控制体(图 3 所示虚线部

分),其 x 方向上的动量方程为:

$$p_{dl}(i) - p_{dr}(i) = \Delta p_{d\text{沿程}} + \rho_d k_d [V_{dr}^2(i) - V_{dl}^2(i)]$$

$$i = 1, 2, \dots, n \quad (1)$$

式中: $\Delta p_{d\text{沿程}}$ —分配集箱沿程摩擦阻力; k_d —分配集箱静压变化系数。

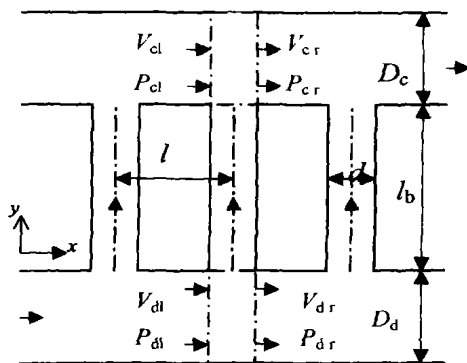


图 3 分配集箱结构图

3.2 汇集集箱中支管部分的动量方程

$$p_{cl}(i) - p_{cr}(i) = \Delta p_{c\text{沿程}} + \rho_c k_c [V_{cr}^2(i) - V_{cl}^2(i)]$$

$$i = 1, 2, \dots, n \quad (2)$$

式中: $\Delta p_{c\text{沿程}}$ —汇集集箱沿程摩擦阻力; k_c —汇集集箱静压变化系数。

3.3 分配集箱中两支管间部分的动量方程

对于第 $i-1$ 根到 i 根支管间的控制体,有:

$$p_{dl}(i) - p_{dr}(i-1) = \lambda_{dl}(i) \frac{l-d}{D_d} \times \frac{1}{2} \rho_d V_{dl}^2(i)$$

$$i = 2, 3, \dots, n \quad (3)$$

3.4 汇集集箱中两支管间部分的动量方程

$$p_{cl}(i) - p_{cr}(i-1) = \lambda_{cl}(i) \frac{l-d}{D_c} \times \frac{1}{2} \rho_c V_{cl}^2(i)$$

$$i = 2, 3, \dots, n \quad (4)$$

3.5 支管部分伯努利方程

$$\frac{1}{2} [p_{dl}(i) + p_{dr}(i)] = \frac{1}{2} [p_{cl}(i) + p_{cr}(i)] +$$

$$(C_r + C_c + \lambda_b(i) \frac{l_b}{d}) \frac{1}{2} \rho_b V_b^2(i)$$

$$i = 1, 2, \dots, n; \quad (5)$$

式中: C_r 、 C_c —支管入口和出口阻力系数; V_b —并联支管内流速。

利用式(1)~式(5)和分配集箱、汇集集箱的连续性方程及相应的边界条件,通过迭代法可求出并联管组的流量分配。

4 试验结果分析

在对试验结果进行分析时, 利用并联支管内的流量分配系数 η_i 来评价介质在分配集箱并联支管内流量分配的均匀性。

$$\eta_i = Q_i / Q \times 100\%$$
 (6)

式中: η_i —第 i 根支管的流量分配系数;

Q_i —第 i 根支管的质量流量;

Q —各支管的平均质量流量。

4.1 质量流速对流量分配的影响

图 4 是分配集箱内工质压力 $p=25\text{ MPa}$, 温度 $t=15\text{ }^\circ\text{C}$ 时, 质量流速对分配集箱垂直水冷壁管内流量分配不均匀性的影响。由图 4 可知, 在分配集箱引入管的质量流速较小时, 垂直水冷壁管内的流量分配不均匀性较大。例如, 分配集箱引入管的质量流速 $G=400\text{ kg}/(\text{m}^2\cdot\text{s})$ 时, 其流量分配不均匀性达到 10%。随着引入管内的质量流速的增加, 垂直水冷壁管内的流量分配均匀性增加, 而且, 当引入管内的质量流速增加到一定值后, 再增加引入管的质量流速时, 质量流速对垂直水冷壁管内流量分配不均匀性的影响很小。本试验中, 当引入管的质量流速 $G\geq 800\text{ kg}/(\text{m}^2\cdot\text{s})$ 时, 质量流速对垂直水冷壁管内流量分配不均匀性的影响较小, 其流量分配不均匀小于 4%。

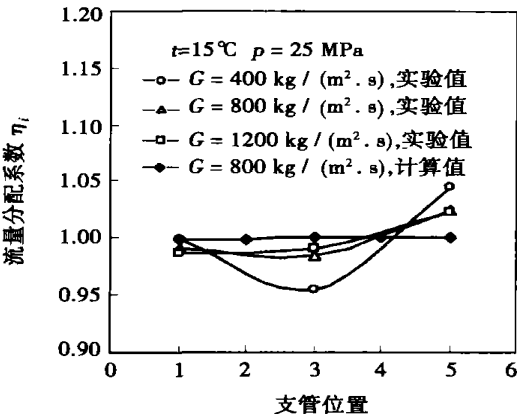


图 4 质量流速对流量分配的影响

图 5 是分配集箱内介质压力 $p=23\text{ MPa}$, 温度 $t=15\text{ }^\circ\text{C}$ 时, 质量流速对分配集箱垂直水冷壁管内流量分配不均匀性的影响。其试验结果与 $p=25\text{ MPa}$, 温度 $t=15\text{ }^\circ\text{C}$ 时的试验结果类似。而且随着压力的增加, 垂直水冷壁管内流量分配的均匀性增加。

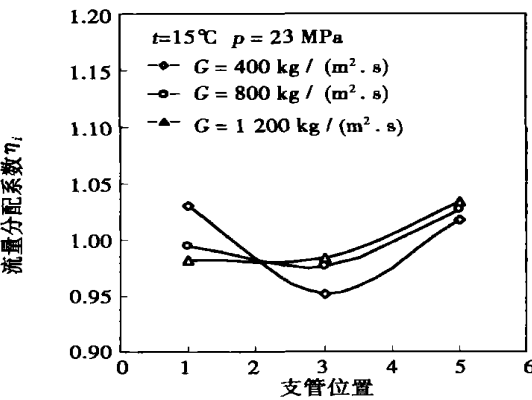


图 5 质量流速对流量分配的影响

4.2 工质温度对流量分配的影响

图 6 为分配集箱内工质压力 $p=25\text{ MPa}$, 质量流速 $G=1200\text{ kg}/(\text{m}^2\cdot\text{s})$ 时, 工质温度对分配集箱垂直水冷壁管内流量分配不均匀性的影响。试验表明, 在工质温度小于 $350\text{ }^\circ\text{C}$ 时, 工质温度对分配集箱垂直水冷壁管内流量分配的不均匀性的影响很小; 但在拟临界点温度 $384\text{ }^\circ\text{C}$ (压力 $p=25\text{ MPa}$ 时) 附近处流量分配的不均匀性有一明显的增加。出现这种现象的原因是超临界压力下水在拟临界点之前, 其物性随温度的变化较小, 但在拟临界点附近, 水的物性发生了显著的变化。可以预见, 随着压力的升高, 这种并联支管内流量分配不均匀性在拟临界点附近的阶跃增加现象变得不明显, 这是因为在超临界压力下, 随着超临界压力的增加, 拟临界点处物性的变化幅度减少。

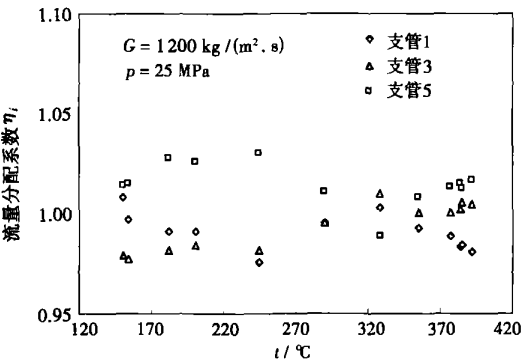


图 6 工质温度对流量分配的影响

5 试验结果与理论分析的比较

利用上述离散模型通过迭代法可以计算出分配集箱垂直水冷壁管内的流量分配, 其结果如图 4 和

图 7 所示。由图可知, 分配集箱垂直水冷壁管内流量分配的试验结果与计算结果偏差较小, 在本试验中, 其偏差在 10% 以内。当流量较小时(例如图 4 中 $G=800 \text{ kg}/(\text{m}^2 \cdot \text{s})$), 在靠近分配集箱进口处的第一根支管的流量比相邻支管内流量大。出现这种现象的原因是分配集箱为从最底部径向引入, 并联支管从分配集箱中部侧面水平引出之后再垂直向上, 而且, 第一根支管的位置离引入管很近。当分配集箱引入管内的流量较小时, 进入分配集箱内介质的动量相对较小, 故进入第一根支管的流量比相邻支管的流量大。当分配集箱引入管的质量流速较大时(例如 $G=1200 \text{ kg}/(\text{m}^2 \cdot \text{s})$), 进入分配集箱内的介质的动量较大, 工作介质进入集箱后更容易沿轴向流动, 此时的流量分配规律与计算结果完全一致, 如图 7 所示。600 MW 超临界直流锅炉在超临界压力下运行时, 分配集箱引入管的质量流速大于 $1200 \text{ kg}/(\text{m}^2 \cdot \text{s})$, 所以利用上述离散模型计算分配集箱垂直水冷壁管内的流量分配可以得到较满意的结果。

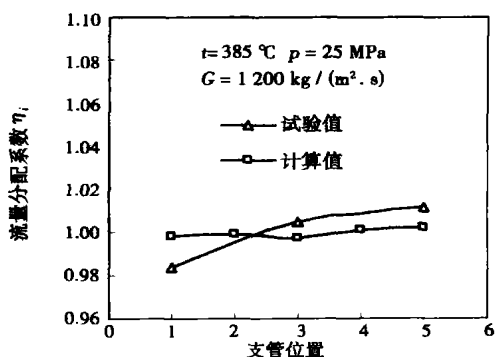


图 7 计算值与试验值的比较

6 结 论

(1) 随着分配集箱引入管内的质量流速的增加, 垂直水冷壁管内的流量分配均匀性增加; 当引入管内的质量流速增加到一定值后, 质量流速对垂直水冷壁管内流量分配不均匀性的影响很小。

(2) 在工质温度小于 350°C 时, 工质温度对分配集箱垂直水冷壁管内流量分配的不均匀性的影响很小; 但在拟临界点温度 384°C (压力 $p=25 \text{ MPa}$ 时) 附近流量分配的不均匀性有一明显的增加。

(3) 采用离散模型计算分配集箱并联支管内的流量分配, 其计算结果与试验值吻合较好; 在分配集箱引入管质量流速较大时, 其误差在 10% 以内。

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(何静芳 编辑)

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when the water quality does not seriously deviate from the design regime, the accumulative tube-plugging rate can be chosen as the status parameter for the on-condition replacement with the decision-making threshold value being set at 1.28%. When the water quality deviates seriously from the design regime, the frequency of accumulative tube-plugging and the failure rate of the current year can be chosen as the status parameter with the decision-making threshold value being the accumulative failure frequency amounting to 20.4 times and the failure rate of the current year being set at 3.95 times/year. Compared with the currently prevailing maintenance modes, the optimized maintenance modes can reduce the operation and maintenance costs by 34%. **Key words:** power plant condensers, RCM analysis, maintenance decision-making, replacement based on specific conditions

内置稳燃热岛燃气锅炉内流动与传热数值模拟 = **Numerical Simulation in the Flow and Heat Transfer in a Gas-fired Boiler with a Built-in Stable-combustion Heat Island** [刊, 汉] / OU Jian-ping, MA Ai-dun (Energy Source and Power Engineering College under the Central South University, Changsha, Hunan, China, Post Code: 410083), LAI Chao-bin, DENG Ren-hua (Xinyu Iron and Steel Co. Ltd., Xinyu, Jiangxi, China, Post Code: 338001) // Journal of Engineering for Thermal Energy & Power. — 2006, 21(3). — 291 ~ 294

With a gas-fired boiler provided with a built-in stable-combustion heat island serving as an object of study and by making use of CFD software PHOENICS coupled with the in-boiler fluid flow, combustion and heat transfer process, a numerical simulation analysis has been performed of the gas flow and heat transfer characteristics of the boiler. The impact of an ignition-aid burner operating condition and an annular stable-combustion heat island on the gas flow and heat transfer process in the boiler was studied with a comparison and verification being made in production practice. The results of the study indicate that the corner-tangential layout of the burners and the presence of an annular heat island in the boiler are conducive to the stable combustion and the formation of tangential flow modes in the boiler, enhancing the agitation of flue gases in the boiler and making the furnace temperature distribution more uniform. As a result, the heat exchange efficiency of the heating surfaces in the furnace has been improved. Through an adjustment of the location of ignition-aid burners the stable combustion of a low heat value gas-fired boiler has been realized. The research results can serve as a guide during the design improvement and production organization of blast furnace gas-fired boilers. **Key words:** boiler, blast furnace gas, stable combustion-based heat island, flow field, heat transfer, numerical simulation

燃油锅炉改烧瓦斯气炉内流动和燃烧过程的数值模拟 = **Numerical Simulation of the Flow and Combustion Process of an Oil-fired Boiler Being Converted to Burn Gas** [刊, 汉] / LIU Ya-qin, LI Su-fen (Power Engineering Department, Dalian University of Science and Technology, Dalian, Liaoning, China, Post Code: 116024), ZHANG Li (Dalian University, Dalian, Liaoning, China, Post Code: 116024) // Journal of Engineering for Thermal Energy & Power. — 2006, 21(3). — 295 ~ 298, 302

An oil-fired boiler was converted to burn gas. To analyze the change of in-boiler flow and combustion conditions, the authors have conducted a three-dimensional numerical simulation by using software Fluent. A “Realizable $k-\epsilon$ ” model was employed to simulate the turbulent flow with a swirling one, while a PDF model used for the simulation of turbulent flow combustion and a P1 model for the simulation of radiation. Through calculations the distribution of in-boiler flow field, temperature field and heat-flux densities along the height were obtained. The calculation results are of major theoretical significance for guiding the operation of gas-fired boilers and their modification. **Key words:** gas combustion, numerical simulation, flow field, temperature field, heat-flux density

超临界压力下水冷壁中间集箱分配特性的研究 = **An Investigation on the Flow Distribution Characteristics of a Water-wall Intermediate Header at a Supercritical Pressure** [刊, 汉] / ZHU Yu-qin, BI Qin-cheng, CHEN Ting-kuan

(State Key Laboratory of Power Engineering Multi-phase Flow under the Xi'an Jiaotong University, Xi'an, Shanxi, China, Post Code: 710049)// Journal of Engineering for Thermal Energy &Power. — 2006, 21(3). — 299~302

An investigation was conducted of the flow distribution characteristics of distribution header water-wall tubes under a supercritical pressure for a home-made 600 MW once-through boiler. The test parameters can be listed as follows: pressure $p=23\sim25$ MPa, mass flow rate $G=400\sim1200$ kg/(m²·s), working medium temperature $t=10\sim400$ °C. An experimental study has been conducted of the impact of working medium pressure, mass flow rate and working medium temperature on the vertical water-wall tube flow distribution characteristics of the distribution header. The test results show that with an increase in mass flow rate, the uniformity of flow distribution among the vertical water-wall tubes could be enhanced. The non-uniformity of flow distribution will undergo a step increase near the quasi-critical points. Moreover, with an increasing pressure, the above-mentioned step increase will become weaker. By employing a discrete model of the parallel-connected branch tubes of the distribution header, the flow distribution among the distribution header vertical water-wall tubes was calculated and the calculation results are in good agreement with the test ones. **Key words:** once-through boiler, supercritical pressure, distribution header, vertical water-wall tubes

USC 直流炉水冷壁壁温监测有限元分析 = **Finite Element Analysis of the Monitoring of Water-wall Water Temperatures in an Ultra-supercritical-pressure Once-through Boiler**[刊, 汉]/WANG Hong-yue, BI Xiao-long, SI Fengqi, et al (Power Engineering Department of Southeast University, Nanjing, Jiangsu, China, Post Code: 210096)// Journal of Engineering for Thermal Energy &Power. — 2006, 21(3). — 303~306, 310

It has all along been rather difficult to realize an on-line monitoring of the hazardous-point wall temperatures of a flame-facing membrane wall in an ultra-supercritical-pressure once-through boiler. Based on a finite-element analysis theory, the authors have come up with a method for the numerical simulation of water-wall cross-section two-dimensional temperature field for the on-line temperature field of a 900 MW ultra-supercritical-pressure utility boiler water wall. Through a theoretical analysis and an experimental verification it has been found that the numerical simulation features a solution of high precision and good confidence level, providing a new monitoring method for the indirect measurement of hazardous-point temperatures in the flame-facing water wall of an ultra-supercritical-pressure once-through boiler. **Key words:** membrane wall, finite element, wall temperature, on-line monitoring, simulation

轮南电站燃气轮发电机组运行方式的试验研究 = **Experimental Study of Operation Modes for Gas Turbine Generator Units at Lun-nan Power Station**[刊, 汉]/CHEN Ren-gui, YUAN Jun, HUANG Xin (Oil and Gas Production Technical Service Department of Tarim Oil Field, Korla, Xinjiang, China, Post Code: 841000), WU Bin (Post-graduate Department of Northeast College of Electric Power, Jilin, China, Post Code: 132012)// Journal of Engineering for Thermal Energy &Power. — 2006, 21(3). — 307~310

Through an analysis of the relevant parameters associated with the process of dynamic-abrupt rise in rotation speed of Lun-nan Power Station gas turbine unit after a load rejection, the dynamic characteristics of the unit were compared when the latter assumes the following three speed control modes: droop control, zero-droop control, and droop and zero-droop mixed control. On the basis of the specific features of the gas turbine unit itself and the current status of isolated electric grid operation of the power station it is recommended that the power station should adopt a droop speed control mode. **Key words:** load rejection, speed control mode, droop control, zero-droop control

CFB 锅炉水冷排渣余热利用的分析与优化 = **An Analysis and Optimization of Waste Heat Utilization Involving Water-cooled Ash-slag Discharged from CFB (Circulating Fluidized Bed) Boilers**[刊, 汉]/ZHANG Ning, SUN