

# 600 MW 燃煤机组锅炉大比例掺烧褐煤的设备改造

王六虎,王 荣,王晓风,范国强  
(内蒙古京隆发电有限责任公司,内蒙古 丰镇 012100)

**摘 要:** 褐煤内水分大、热值低,大量掺烧会出现磨煤机干燥出力不足等一系列问题,严重影响制粉系统的安全运行。通过对空预器改转向、扩风仓、安装软密封及磨煤机喷嘴环扩容等进行一系列改造,使磨煤机入口风温进一步提高、磨煤机干燥研磨出力明显增加、风机阻力下降,在满足锅炉大比例掺烧褐煤要求的同时还可降低风机与磨煤机电耗、减少一次风机失速的危险,为企业带来巨大的经济效益,可为掺烧褐煤的火电厂提供一定的借鉴。

**关 键 词:** 600 MW 燃煤机组; 锅炉; 磨煤机喷嘴; 空预器改造; 褐煤掺烧

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## 引 言

近年来,受燃煤供应紧张及价格持续上涨等不利因素影响,越来越多的火力发电企业出现亏损。褐煤价格相对较低,大量掺烧可有效降低发电成本,缓解企业经营压力,但褐煤内水分大热值低,大量掺烧会引起制粉系统干燥出力不足、煤粉管堵塞、轴流式一次风机阻力高、流量低、风机易失速等一系列问题,严重影响机组的安全运行。因此,有必要对原有设备进行改造,在保证设备安全稳定运行的前提下满足锅炉大比例掺烧褐煤的要求,进一步降低发电成本。

## 1 设备概况

内蒙古京隆发电公司 2 × 600 MW 亚临界直接空冷机组,采用中速磨煤机冷一次风正压直吹式制粉系统,磨煤机为 ZGM113G 中速辊式磨煤机,最大通风量为 100.87 t/h,使用设计煤种标准出力为 64.66 t/h ( $R_{90} = 20\%$   $HGI = 50$   $WY = 10\%$ ),每台炉配 6 台磨煤机,燃烧设计煤种时 5 台运行,1 台备用。锅炉设计煤种为准格尔矿煤,校核煤种为晋北

代表煤。

## 2 改造方案

掺烧褐煤最直接的影响是磨煤机出口风温较低,易引起煤粉管堵塞、一次风率高易引起风机失速,因此改造思路主要以提高热一次风温、降低一次风阻力、降低空预器漏风等为目的。京隆发电公司在充分调研论证的基础上,提出对磨煤机喷嘴环进行扩容改造,增大磨煤机通流面积及通风量,有效降低一次风机阻力,避免轴流风机失速;通过空预器改变转向、扩大一次风风仓面积及增加径向软密封,使空预器出口热一次风温提高 30℃ 左右,空预器漏风率大幅下降,有效提高磨煤机干燥、研磨出力,进一步满足大比例掺烧褐煤的要求。

### 2.1 磨煤机喷嘴环改造

传统 ZGM113G 型中速磨煤机喷嘴环为铸件式,喷嘴环厚度较厚,热一次风通流面积小,通风阻力大,喷嘴环磨损严重,每隔半年左右需进行堆焊。静环也为铸件式,直接焊在磨煤机筒体上,不易更换,长期运行一次风会将静环吹穿,补焊非常困难,有可能会发生动静环之间发生摩擦,影响磨煤机正常运行,甚至发生严重事故。

新型旋转喷嘴环,喷嘴环与磨盘采用分体式结构。动静间隙、喷嘴环型线及厚度根据磨煤机运行参数重新设计计算,静环采用可更换式安装的方法,通过螺栓与焊接在筒体的法兰连接紧固。动环、静环均采用耐磨、耐高温的特殊材料铸造而成,使用寿命达 18 000 h 以上。改造具体部位如下:

(1) 静环由原来的铸件变为铆焊件,不影响衬板、喷嘴的更换。静环沿垂直方向向外倾斜 15°,便于形成旋转风,减少机壳磨损。静环外壁贴 UP 板

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作者简介: 王六虎(1973 -),男,内蒙古包头人,内蒙古京隆发电有限责任公司高级工程师。

耐磨材料,可以有效延长静环的使用寿命。

(2) 旋转喷嘴由原来的铸件变为焊接件,喷嘴叶片的厚度由原来的 65 mm 减为 18 mm,通流面积由  $0.56 \text{ m}^2$  增大到  $1.01 \text{ m}^2$ ,可有效增大热一次风通流面积。叶片内倾斜角度  $40^\circ$ ,冲刷磨损区采用耐磨设计。材质采用 16Mn 淬火,硬度达到 HB330 以上。除衬板外的动环静环等设备使用寿命达 18 000 h ( $K_e \leq 2.5$ ) 以上。

(3) 辊套和衬板型线进行了改进,辊套直径为  $\phi 1\ 810 \text{ mm}$ ,辊套外圆为 R440 mm,衬板弧线为 R540 mm。此种改进增大了碾磨面积,同时便于石子煤的顺畅排出。

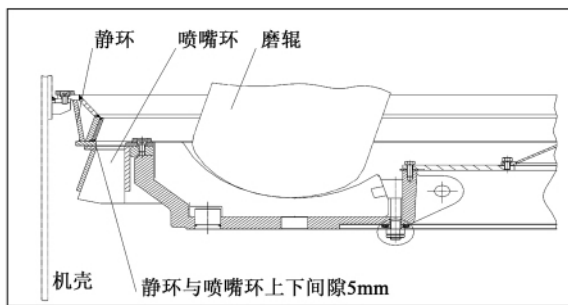


图1 改造后的喷嘴环示意图

Fig. 1 Schematic diagram of the nozzle ring after reconstruction

当静环、动环(包括磨盘)全部更换时,主要更换部件有:磨环托盘、防磨衬板、旋转喷嘴环、静环、分段法兰、支架等。

## 2.2 空预器系列改造

空预器改造主要有3部分,包括转动方向的改变,一二次风仓角度的改变及加装软密封。

### 2.2.1 扩大一次风风仓角度改造

原一次风仓角度为  $50^\circ$ ,为增大一次风量,通过计算将一次风仓扩为  $65^\circ$ ,一次风量可大幅增加且不影响锅炉效率。具体改造如下:

(1) 拆除径向密封片、轴向密封片和一次风侧部分旁路密封片、角钢;割除空预器冷端一次风侧刚性环及壳体;拆除冷端一次风组件,平移一次风梁位置,改成  $65^\circ$ ;安装修复冷端一次风组件。

(2) 割除空预器热端静密封、一次风侧刚性环及壳体;拆除热端一次风组件、漏风系统,平移一次风位置,改成  $65^\circ$ ;安装修复热端一次风组件及漏风控制系统。

(3) 调整扇形板及漏风控制系统。

### 2.2.2 空预器转动方向改造

空预器改转向,旋转方向由原来的反转改为正转,即空预器旋转方向由原来的“烟气侧→二次风→一次风”改为“烟气侧→一次风→二次风”,空预器旋转时先通过一次风侧再经过二次风侧,可以有效提高一次风出口风温。因空预器有三套驱动装置,主电机、辅助电机和气动发动机驱动,所以具体改动时分3步进行。主电机、辅电机改转向时只需将接线反接即实现了电机的反转。辅助电机和气动发动机都装有超越离合器,改造时将旧超越离合器拆下检查无损坏后直接反装即可,如损坏需更换新超越离合器,安装方向与原方向相反,这样,空预器启动时,就实现了主电机、辅电机和气动发动机3种驱动装置转向的改变。

### 2.2.3 软密封改造

软密封是在径向密封片(常规设计配置)后部配置双道消除阻流片,兼具迷宫效应,起到减小漏风、延长软密封寿命、方便维护调整的作用,软密封为接触式密封,软密封片和径向密封片分装于径向隔板两侧,材质为低合金耐高温腐蚀考登钢,可在最高  $450^\circ\text{C}$  下长期运行,不会出现软化或残留变形。软密封片上的调节开孔为垂直式,可以保证反复调整间隙 4~5 次,一旦出现过量磨损后可以再次调整位置,每年只需调整 1 次左右,无需频繁更换密封片。

## 3 改造效果评价

### 3.1 磨煤机喷嘴改造效果评价

新型喷嘴环角度、型线及喉口流速的改进,有效地改善了磨煤机内部的空气动力场,大幅度地降低了通风流速,通风阻力也相应降低,使得进入磨煤机内部的一次风分配更为合理,风粉混合物更趋于均匀,有效提高煤粉分离器的效率和磨煤机出力。

由于改造后的静环与喷嘴环都采用了耐磨材料,因此磨损情况与改造前相比效果非常明显。增大通流面积使得喷嘴环喉口部位流速较大幅度降低。因此一次风速降低有效减小了喷嘴环喉口部位的冲刷磨损,连续运行 3 000 h 后检查发现静环及喷嘴环壁厚磨损几乎为零,未改造前运行 3 000 h 后需进行补焊。

表 1 磨煤机喷嘴环改造前后数据对比(风量 100 t/h)

Tab. 1 Contrast of the data before and after the modification of the nozzle ring of the coal mill

项目	原设计	改造前	改造后
入口气体体积流量 $V_{PA} / m^3 \cdot s^{-1}$	41.40	46.80	55.10
叶片厚度(切向) $T/mm$	65	65	18
叶片数量 $n/\text{个}$	40	40	36
圆角 $r/mm$	10	10	5
整圈喷嘴口通风面积 $A_{ring}/m^2$	0.406	0.406	0.870
间隙通风面积 $A_{gap}/m^2$	0.083	0.083	0.030
总通风面积 $A_{total}/m^2$	0.489	0.56	1.01
100%风量时喷嘴流速 $v/m \cdot s^{-1}$	84.6	95.7	61.2

由于采用改造后的旋转喷嘴环,热一次风通流面积增大,通风阻力大为下降,一次风机预磨煤机电耗也明显下将,煤粉管磨损情况也有所减轻,不会频繁地发生漏粉现象,不仅使检修周期大大延长,而且还减少了维护费用,生产现场的安全文明生产水平得到进一步提高。

表 2 不同工况下改造前后磨煤机运行参数对比

Tab. 2 Contrast of the operating parameters of the coal mill before and after modification under various operating conditions

项目	工况一		工况二	
	改造后	改造前	改造后	改造前
磨煤机出力 $/ t \cdot h^{-1}$	51.8	46.8	55.5	45.7
磨煤机电流/A	86.8	101.4	85.2	93.3
磨煤机入口风温/ $^{\circ}C$	298	268	308	275
磨煤机出口风温/ $^{\circ}C$	53	53	57	55
入口一次风量 $/ t \cdot h^{-1}$	94.0	79.0	97.6	88.9
入口一次风压/kPa	7.294	7.594	8.498	8.980

### 3.2 空预器改造效果评价

空预器进行系列改造后,一次风温提高约 30  $^{\circ}C$ ,磨煤机干燥出力明显增加,研磨出力也增加约 5 ~ 10 t/h。加装软密封后,空预器启动初期电流较之前增大 5 ~ 10 A。在达到满负荷运行 48 ~ 96 h 后,空预器的软密封磨合完成,运行电流和未装软密封时一致,偏差小于 1 A。漏风率由之前的 9% 降至 5.4%。

表 3 空预器系列改造后参数对比情况

Tab. 3 Contrast of the parameters of an air preheater before and after a series of modification

名称	改造前	改造后
入口一次风温/ $^{\circ}C$	25/26	25/26
出口一次风温/ $^{\circ}C$	309/305	332/332
入口二次风温/ $^{\circ}C$	25/26	25/26
出口二次风温/ $^{\circ}C$	318/317	310/315
入口烟温/ $^{\circ}C$	356/358	358/357
排烟温度/ $^{\circ}C$	130/135	132/135
送风机电流/A	250/249	222/222
一次风机电流/A	109/108	97/99

## 4 改造后经济性分析

### 4.1 磨煤机喷嘴环改造经济性分析

2号炉 C 磨煤机喷嘴环改造费用共 64 万元。静环、喷嘴环、磨盘等全部更换,材料费用共 58 万元,人工费用约 8 万。如在旧磨盘的基础上改造,磨盘不用更换,只更换喷嘴环及静环,总费用约 54 万元。2号炉 3 台磨煤机改造总费用共 186 万。

将准煤与褐煤按 1:1 比例掺烧,C 磨的平均磨煤电耗为 8.767  $kW \cdot h/t$ ,F 磨的平均磨煤电耗为 11.258  $kW \cdot h/t$ ,每年运行 8 000 h 计算,C 磨每年可节约厂用电约 125.676 万  $kW \cdot h$ 。按公司上网电价(华北网)0.3731 元/( $kW \cdot h$ )计算,每年可节约 46.89 万元。同时,燃用低成本褐煤,与标煤单价比褐煤高 48.08 元/t、热值为 19 520  $kJ/kg$  的乌海煤相比,一年还可节约燃料成本  $48.08 \times 14.35 \times 8000 = 51.92$  万元(其中 14.35 t 为 22.5 t/h 掺烧的褐煤按发热量折合成乌海煤的量)。两项一年可节约费用 98.81 万元,每台炉三台磨煤机进行改造,一年节约费用 296.43 万元。动静环设备寿命按 18 000 h 算,一个更换周期内可节约费用为  $296.43 \times 18000 \div 8000 - 186 = 480.97$  万元。单台炉每年可节约成本约 480.97 万元。 $186 \div 480.97 = 0.387$  只需 4 个多月即可收回成本。

### 4.2 空预器改造的经济性分析

改造前,两台空预器漏风率平均在 9% 左右,通过安装软密封后,两台空预器漏风率降至 5.4%。平均负荷下一次风机、送风机电流分别降低 10、30

A. 根据  $W = \sqrt{3}UI \cdot \cos\varphi$  送风机电压 3 000 V, 一次风机电压 10 000 V, 每年运行 800 小时计算, 华北网上网电价按 0.3731 元/(kW·h) 计算: 一次风机每年节省 95.21 万元; 送风机每年节省 85.48 万元; 空预器改造后风机降耗产生的效益:  $95.21 + 85.48 = 180.69$ (万元)。

通过对锅炉设备进行的一系列改造, 完全满足了大比例掺烧褐煤的需要。2011 年京隆发电公司褐煤掺烧比例近 40%, 最高达 61.3%, 全年共掺烧褐煤 81.1 万吨, 节约燃料成本约 6 283 万元, 加上设备改造降低电耗产生的经济效益, 全年共节约成本  $480.97 + 180.69 + 6 283 = 6 944.66$  万元, 为企业进一步扭亏奠定了坚实的基础。

## 5 结 语

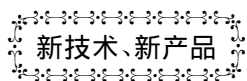
掺烧低成本褐煤, 解决火电厂燃煤不足的难题, 同时还节省大量的燃料成本, 为企业带来巨大的经济效益。虽然掺烧褐煤会给锅炉的安全稳定运行带来诸多不利影响, 但通过进行合理的设备改造, 不仅满足了大比例掺烧褐煤的要求, 同时降低了磨煤机、风机电耗, 延长了煤粉管道设备使用寿命, 为企业带来了可观的收益。面对国内火电行业不断亏损及区域电网负荷整体大幅下滑的不利局面, 京隆发电公司积极探索、勇于创新, 走出了一条属于自己的褐煤掺烧之路, 并为大比例掺烧褐煤进行了一系列设备

改造, 可为正在或即将掺烧褐煤的火力发电企业提供宝贵的经验。

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( 辉 编辑)



新技术、新产品

## Frame 6FA 驱动三个联合生产装置

据《Gas Turbine World》2012 年 9—10 月刊报道, GE 已经得到一份合同, 为中国浙江省的三个电站供应 5 台 Frame 6FA 燃气轮机发电机组。

采用燃气轮机联合生产装置来代替较低效率烧煤锅炉, 可减少对环境的影响并增加地区的能源效率。

以联合循环方式运行的每个装置都将生产高达 230 MW 功率, 热效率为 53.5%; 如果以联合生产方式运行时可达到接近 80% 的热效率。而类似功率等级的烧煤装置的热效率仅为 30%。

在 2012 年 12 月它们投入商业运行时, 将生产约 575 MW 总的电力, 并为在该区域的有关工业提供过程热源。

来自西气东输管线的天然气将是这三台装置的主燃料。

( 吉桂明 摘译)

The magnitude of the flammable content of fly ash represents one of the important factors influencing the efficiency of a boiler and plays an important role in economic operation of the boiler. The authors optimized the linking weight value and threshold one between the nodes of a BP neural network by using the PSO (particle swarm optimization) algorithm and established a BP neural network-based model optimized by using the PSO algorithm (called as a PSO-BP model for short). The model can thoroughly give a full play of both overall optimization searching ability of the particle swarm optimization algorithm and the local searching edge of the BP algorithm. The operating parameters of a 670 t/h boiler were used to predict the flammable content of the flying ash. It has been found that compared with the BP neural network based model, the PSO-BP model is more precise and faster to come to a converging point, thus offering a feasible method for analyzing and predicting the flammable content of fly ash in large-sized utility boilers. **Key words:** BP neural network, flammable in fly ash, optimization, modeling

1 000 MW 燃煤机组的热经济学分析 = **Thermoeconomic Analysis of a 1 000 MW Coal-fired Power Generation Unit** [刊, 汉] CHENG Wei-liang, JI Hui, DI An (College of Energy Power and Mechanical Engineering, North China University of Electric Power, Beijing, China, Post Code: 102206) // Journal of Engineering for Thermal Energy & Power. - 2013, 28(2). - 187 ~ 191

To analyze in a comprehensive way the technical and economic operation characteristics of a large-sized thermal power generation unit, established was an analytic model based on the matrix mode thermoeconomics with a 1000 MW large-sized coal-fired unit serving as the object of study. By employing a thermoeconomic performance calculation software developed, to calculate, analyze and optimize the corresponding indexes were realized and at the meantime, a concept of average thermoeconomic unit cost was presented. It has been found that the exergy economic coefficients of the feedwater pumps and boilers are relatively small, indicating that their exergy losses take up relatively big proportions. The exergy economic coefficient of No. 2 high pressure heater is very high. With an increase of the live steam pressure, the average thermoeconomic unit cost will gradually decrease. With a rise of the live steam temperature, such a cost will decrease relatively quickly. When the live steam temperature or reheat temperature is 597 °C, such a cost will be down to its minimum value. **Key words:** thermoeconomics, evaluation index, cost analysis, average unit thermoeconomic cost, exergy economic coefficient

600 MW 燃煤机组锅炉大比例掺烧褐煤的设备改造 = **Equipment Modification of a 600 MW Coal-fired Boiler Mixing-dilution Burning With Lignite at a Large Proportion** [刊, 汉] WANG Liu-hu, WANG Rong, WANG Xiao-feng, et al (Inner Mongolia Jinglong Power Generation Co. Ltd., Fengzhen, China, Post Code: 012100) // Journal of Engineering for Thermal Energy & Power. - 2013, 28(2). - 192 ~ 195

Due to a big water content and low heating value of lignite, its mixing-dilution combustion in a large amount may e-

merge an insufficient drying capacity of the coal mill and a series of problems and seriously influence the safe operation of the pulverized coal milling system. Through a series of modification such as rotation direction change ,air chamber enlargement ,soft seal installation and capacity enlargement of the nozzle ring of the coal mill ,the air temperature at the inlet of the coal mill was further enhanced ,the drying and milling capacity of the coal mill was conspicuously increased and the resistance of the blower was lowered. At the same time of meeting the requirements for mixing-dilution burning with lignite at a large proportion ,the power consumption rate of the blower and coal mill can be reduced and the risk of the primary air blower starting to stall can be reduced ,thus bringing huge economic benefits to the enterprise and providing certain reference for thermal power plants mixing-dilution burning with lignite.

**Key words:** air preheater modification ,lignite mixing-dilution combustion ,economic benefit

不同水质下铜表面  $\text{CaCO}_3$  污垢初始阶段生长特性 = **Initial Growth Characteristics of the  $\text{CaCO}_3$  Fouling on Copper Surfaces of a Heat Pump Water Heater Under Various Water Qualities** [刊 ,汉] SHENG Jian , ZHANG Hua ZHAO Ping ( College of Energy Source and Power Engineering ,Shanghai University of Science and Technology ,Shanghai ,China ,Post Code: 200093) //Journal of Engineering for Thermal Energy & Power. - 2013 , 28( 2) . - 196 ~ 201

Red copper and brass are deemed as the commonly used materials for the heat exchange between coolants and water in heat pump water heaters. The fouling will be serious at 60 °C. To study the growth characteristics of the  $\text{CaCO}_3$  precipitation crystal fouling on metal surfaces ,in 0.5 and 1.0 mmol/l  $\text{CaCO}_3$  solution respectively ,the weight and microscopic morphology of the fouling were obtained through static state reactions by using weight weighing and SEM ( scanning electronic microscopy) method at various immersing time durations. It has been found that the fouling quantity on the red copper surface is bigger than that on the brass surface and red copper is earlier to form a fouling layer than brass. The fouling quantity in the earlier period at a relatively high concentration of  $\text{Ca}^{2+}$  is less than that at a relatively low concentration of  $\text{Ca}^{2+}$  ,however ,the final fouling quantity at a relatively high concentration is larger than that at a low concentration. The concentration of  $\text{Ca}^{2+}$  will not influence the kind of the crystal and its proportion but the crystal in large sizes will emerge earlier and more but relatively small when the concentration is relatively high. A relatively high pH value will result in a relatively high energy level of the solution system ,increase the impurities ,heighten the molecular activity of the metal surface ,change the ionization balance of  $\text{CaCO}_3$  ,produce more nuclei and promote aragonite to be turned into calcite. The main mechanism governing the formation of the precipitation crystal fouling lies in that the fouling particles will be first formed in the solution from the difficultly dissolved salt molecules and then deposited on the metal surface through deposition but not only formed directly through the surface reactions and adsorption. **Key words:**  $\text{CaCO}_3$  precipitation crystal fouling ,coupon test , crystal morphology ,surface reaction ,particle conglutination