

直接空冷机组真空系统夏季喷淋性能研究

赵洪滨, 谢攀, 吴海霞

(中国石油大学(北京) 机械与储运工程学院, 北京 102249)

摘要: 直接空冷机组真空系统夏季运行背压较高, 严重影响机组的安全与经济运行。本研究对夏季真空系统工况下的喷淋效果进行理论分析, 并通过机组喷淋运行试验对模型进行验证, 获得了不同喷淋工况下的背压变化规律, 并得到了喷水最大蒸发量。研究表明: 当喷水量超过喷水最大蒸发量时, 机组背压变化较小; 在相同喷水量条件下, 机组高负荷、高温运行比低负荷、低温运行时的背压降低效果更明显。本研究可为直接空冷机组夏天高温环境下的安全与经济运行提供理论指导。

关键词: 直接空冷; 运行背压; 夏季喷淋; 喷水量; 性能分析

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引言

我国发电行业主要以燃煤发电为主, 燃煤发电约占电力能源的 70%, 而且短时间内煤电的比例不会发生太大变化。同时由于我国水资源短缺, 严重制约着经济的发展, 全国约有 400 多座城市缺水, 缺水总量约为 400 亿 m^3 ^[1-2]。煤炭和水资源分配不均问题严重制约着我国电力行业的发展。因此, 空冷机组以其节水、运行方便、可靠等优势, 逐渐应用于我国西北富煤缺水地区的发展。

1 直接空冷凝汽器夏季喷淋理论

1.1 直接空冷机组真空系统夏季工况出现的问题

由于环境温度高, 导致入口风温增大, 大大降低直接空冷凝汽器的冷却能力, 使得夏季机组处于高背压运行状态。为了保证机组的安全运行, 只有在损失经济性的基础上降低运行负荷。机组长时间处于高背压和限负荷状态, 严重影响着机组的安全性与经济性^[3-4]。因此, 通过喷淋措施, 降低入口空气温度, 强化直接空冷凝汽器的换热能力, 可有效解决

机组夏季出力受阻问题, 是保证机组安全和经济运行的有效途径之一^[5-7]。

图 1 为直接空冷系统雾化增湿图。从直接空冷系统喷雾增湿原理、喷淋前后机组冷端系统运行性能变化等方面对喷雾增湿法在大型电站直接空冷系统的应用进行了规律性研究。

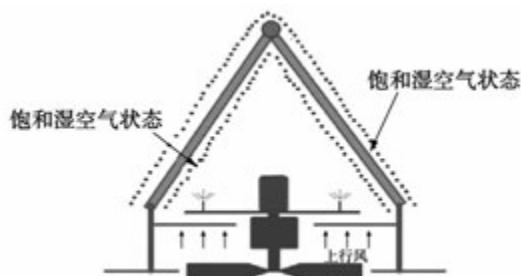


图 1 直接空冷凝汽器雾化增湿示意图

Fig. 1 Schematic diagram of the wetness enhancement through atomization in a direct-air-cooled condenser

1.2 喷淋冷却系统的工作原理

为了防止直接空冷凝汽器结垢, 喷淋水多采用除盐水。喷淋水经过喷嘴雾化进入到空气中, 吸收空气中的大量热量, 迅速蒸发为水蒸气, 在此换热过程中降低了空气的干球温度, 提高了直接空冷凝汽器的冷却能力。

雾化增湿过程如图 2 所示; 图 3 为喷雾增湿前后空气的焓(h) - 湿(d) 图。空气喷淋增湿过程为绝热加湿, 因此喷淋前后湿空气的焓值不变而含湿量和相对湿度增大, 温度减小。

2 直接空冷凝汽器夏季喷淋性能模型

2.1 喷水雾化加湿模型

湿空气的相对湿度 φ 用式(1) 表示:

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作者简介: 赵洪滨(1964-), 男, 山东寿光人, 中国石油大学(北京) 副教授。

$$\varphi = \frac{P_v}{P_s} \quad (1)$$

φ 值介于 0 和 1 之间, 当 $\varphi = 1$ 时, 湿空气达到饱和。 P_v 湿空气中水蒸气分压; 饱和水蒸气压力 p_s 可由式(2) 表示, 单位为 kPa, 其中 t 为空气干球温度。

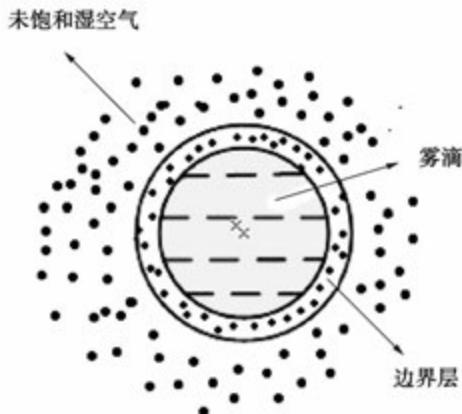


图 2 雾滴与空气间的热湿交换

Fig. 2 Heat and wet steam exchange between the mist droplets and air

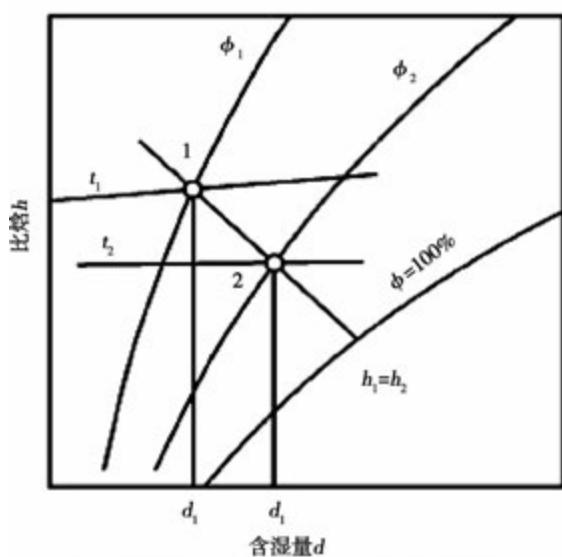


图 3 喷雾增湿前后空气的 $h-d$ 图

Fig. 3 The psychrometric chart of the air before and after the spray humidification

$$p_s = \frac{2}{15} \exp \left[18.5916 - \frac{3991.11}{t + 233.94} \right] \quad (2)$$

1 kg 干空气所带的水蒸气质量为含湿量, 以 d 表示, 单位为 kg(水蒸气)/kg(干空气)。

$$d = 0.622 \frac{\varphi p_s}{p - \varphi p_s} \quad (3)$$

湿空气的比焓 h 表示为:

$$h = 1.005t + d(2501 + 1.86t) \quad (4)$$

据质量守恒, 喷水量等于湿空气含湿量的增加:

$$G_w = m_a(d_2 - d_1) \quad (5)$$

式中: d_1 —喷水前空气的含湿量, kg(水蒸气)/kg(干空气); d_2 —喷水后空气的含湿量, kg(水蒸气)/kg(干空气); m_a —干空气的质量, kg。

据能量守恒, 稳定流动, 且绝热不作外功, 则:

$$m_a h_1 + (d_2 - d_1) m_a h_1 = m_a h_2 \quad (6)$$

式中: h_1 、 h_2 —喷淋前后湿空气的焓值, kJ/kg(干空气); h_1 —喷淋水的焓值, kJ/kg。根据质量守恒与能量守恒, 可以求得喷水后环境温度的变化情况。

2.2 喷淋换热计算模型

喷淋时期, 直接空冷凝汽器管内蒸汽与管外空气进行换热, 可以分为 3 种情况: (1) 未饱和湿空气与直接空冷凝汽器进行换热; (2) 饱和湿空气与直接空冷凝汽器进行换热; (3) 饱和湿空气加水与直接空冷凝汽器进行换热。

管内饱和水蒸气凝结为饱和水的放热量:

$$Q_1 = D_n(h'_n - h'_{sn}) \quad (7)$$

式中: h'_n —喷淋后湿饱和蒸汽焓, kJ/kg; h'_{sn} —喷淋后饱和水焓, kJ/kg; D_n —汽轮机排汽量, kg/s。

与直接空冷凝汽器换热前管外流体为饱和湿空气或未饱和湿空气时, 管外流体的吸热量:

$$Q_2 = (G_a + G_w)c_{p,aw}(t'_{a2} - t'_{a1}) \quad (8)$$

式中: $(G_a + G_w)$ —喷淋后湿空气的质量流量, kg/s; $c_{p,aw}$ —湿空气的比热, kJ/(kg·K); t'_{a1} —喷淋后入口空气温度, °C; t'_{a2} —喷淋后出口空气温度, °C。

与直接空冷凝汽器换热前管外流体为饮和湿空气和喷淋水时, 管外流体吸热量:

$$Q_2 = (G_a + G_{w1})c_{p,aw}(t'_{a2} - t'_{a1}) + G_{w2}c_{p,w}(t'_{a2} - t'_{a1}) \quad (9)$$

$$G_w = G_{w1} + G_{w2} \quad (10)$$

式中: G_{w1} —汽化为水蒸气进入到湿空气中使得湿空气变为饱和状态的喷水量, kg/s; G_{w2} —没有汽化, 温度增加到与环境空气温度相同的那部分喷水量, kg/s; $c_{p,w}$ —喷淋水的比热容, kJ/(kg·K)。

传热量:

$$Q_3 = K'A\Delta t'_m \quad (11)$$

$$\Delta t'_m = \frac{(t'_{s} - t'_{a1}) - (t'_{s} - t'_{a2})}{[\log(t'_{s} - t'_{a1}) / (t'_{s} - t'_{a2})]} \quad (12)$$

式中: K' —喷淋后直接空冷凝汽器传热系数, W/(m²·K); $\Delta t'_{\text{m}}$ —喷淋后直接空冷凝汽器对流平均温差, °C。

根据管内外能量平衡及质量平衡方程可以得出喷水量和喷水后背压变化情况。

3 直接空冷凝汽器喷淋效果分析

喷淋水直接喷入到直接空冷凝汽器 A 型单元下方的空气中,随着喷水雾化量的变化管外空气的组成和温度也在逐渐发生变化。本研究将从以下 3 种情况进行分析,分别得到喷淋加湿条件下喷淋对直接空冷凝汽器性能的影响规律。

3.1 入口空气为饱和湿空气

环境空气为未饱和状态,其相对湿度为 62%,不同工况下使管外空气达到饱和状态的喷水量 G_{w1} 如图 4 所示。图 5 为风机转速为 100% 时,喷淋前后入口风温随环境温度的变化。可以看到,当环境温度为 35 °C, 风机转速为 100% 时,喷水量为 278 t/h 才能使空气达到饱和状态,此时入口风温下降 6.7 °C。且随着风机转速的提高,轴流风机输出的风量逐渐增多,使空气达到饱和状态时所需的喷水量逐渐增大。图 6 表示的是排汽量与背压的关系,喷淋后背压下降,且随着排汽量的升高而增加,当排汽量为 150 和 330 kg/s 时,背压分别下降 3.21 和 5.5 kPa。

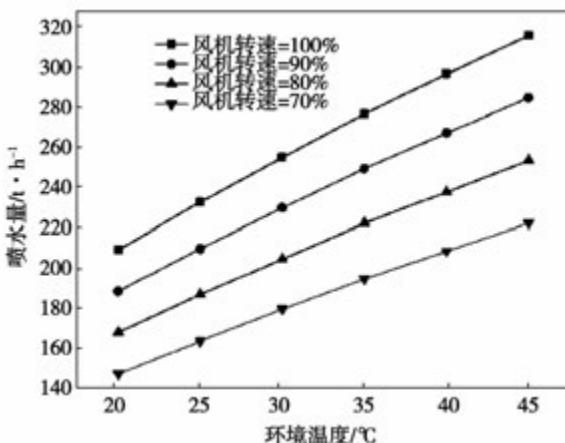


图 4 不同工况下使换热前空气达到饱和状态所需的喷水量

Fig. 4 The water spray quantity made air saturated condition before converter under different conditions

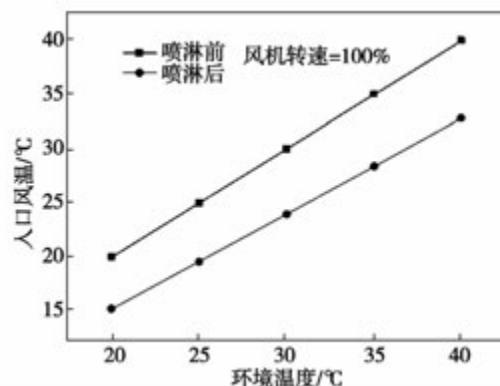


图 5 喷淋前后入口风温随环境温度的变化

Fig. 5 The change of air temperature at inlet with ambient temperature before converter before and after sprinkle

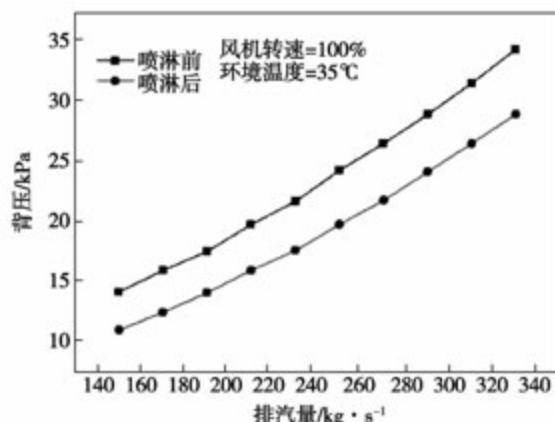


图 6 喷淋前后排汽量 - 背压的关系

Fig. 6 The relationship between turbine exhaust steam flow rate and back-pressure before and after sprinkle

从图 7 中可以看出,环境温度越高,入口空气由未饱和状态变为饱和状态时,背压降低越大,喷淋效果越明显,当环境温度为 20、45 °C 时,喷淋后背压分别下降 2.79、8.5 kPa。

在图 8 中,喷淋前后,不同风机转速背压下降的大小略有不同,且在风机转速较小时,喷淋效果比较明显一些。比如,当风机转速为 70%、100%,背压分别下降 6.74、6.08 kPa。

3.2 出口空气为饱和湿空气

当喷水量等于 G_{w2} 时,出口空气为饱和湿空气,在与直接空冷凝汽器换热过程中,管外流体由水、空气与水蒸气组成,其共同作用与管内蒸汽进行换热。不同环境温度下使得换热后空气达到饱和状态时的

喷水量随排汽量的变化规律如图9所示,喷水量随着环境温度的升高而升高,随着排汽量的增大而增大。

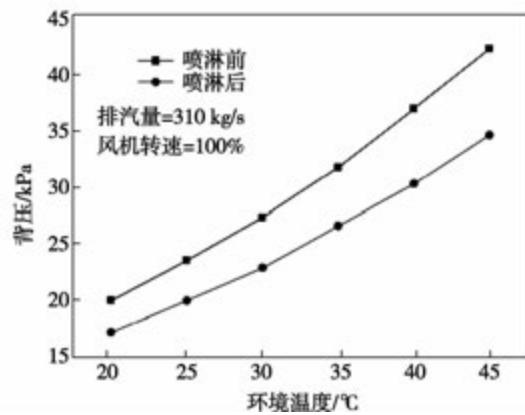


图7 喷淋前后环境温度 - 背压的关系

Fig. 7 The relationship between ambient temperatures and back-pressure before and after sprinkle

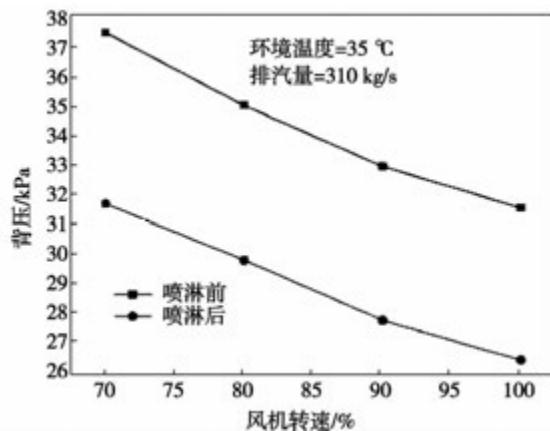


图8 喷淋前后风机转速 - 背压的关系

Fig. 8 The relationship between fan speeds and back-pressure before and after sprinkle

从图10中可以看出,随着排汽量的增加,喷淋前后背压的差值逐渐增大,当 $D_n = 150, 330 \text{ kg/s}$ 时,背压分别下降5.59、17.10 kPa,因此汽机高负荷运行时,采取喷淋措施效果比较明显。

图11表示的是喷淋前后背压随环境温度变化的趋势图,当环境温度大于30 °C时,相对于低温时,喷淋可以明显的降低背压,高温时的喷淋效果比低温时明显。

从图12中看出,喷淋前随着风机转速的增大,背压逐渐降低,在此工况下,相对于环境温度、排汽量对背压的影响,风机转速对背压的影响较小。喷

淋后,在相同的风机转速下,背压明显降低,但风机转速的变化对喷淋后背压的影响较小,风机转速从70%增加到100%,背压只是稍微有所降低。

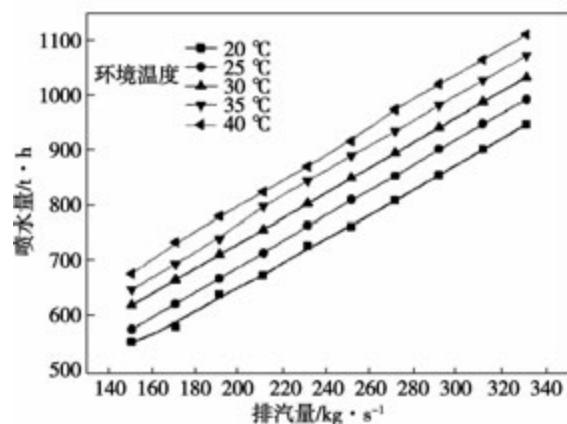


图9 不同工况下使得换热后空气达到饱和状态所需的喷水量

Fig. 9 The water spray quantity made air saturated condition after converter under different conditions

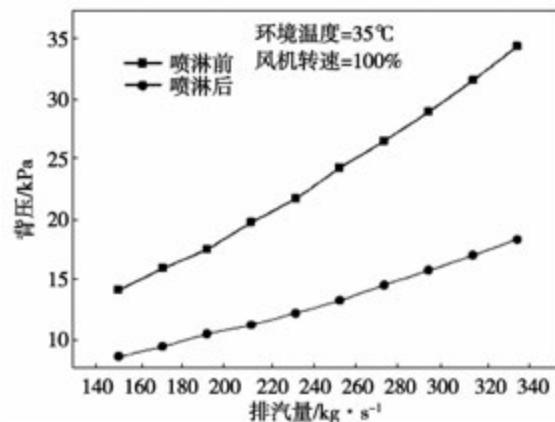


图10 喷淋前后背压 - 排汽量关系

Fig. 10 The relationship between turbine exhaust steam flow rate and back-pressure before and after sprinkle

3.3 喷水量对背压的影响

以使入口空气为饱和湿空气的喷水量和使出口空气为饱和湿空气的喷水量为两个分界点,重点讨论工况下不同喷水量对背压的影响规律。

在图13中,当喷水量小于 G_{w2} ,随着喷水量的增大,出口风温持续降低;当喷水量大于 G_{w2} 时,出口风温变化很小。当喷水量小于 G_{w1} 时,入口风温与出口风温温差最大。随着喷水量的增加,温差逐渐

变小,当喷水量大于 G_{w2} ,温差变化很小, G_{w2} 为当前工况下的喷水最大蒸发量。

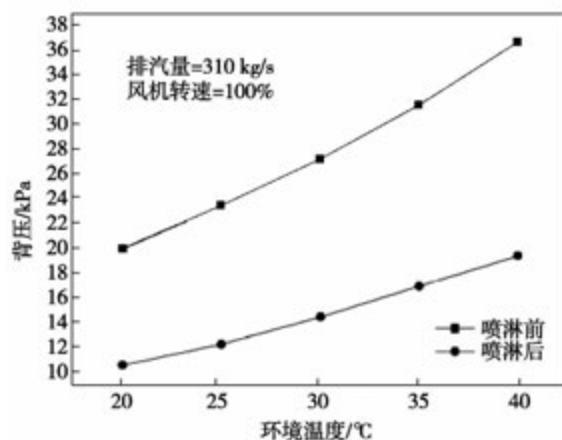


图 11 喷淋前后背压 - 环境温度关系

Fig. 11 The relationship between ambient temperatures and back-pressure before and after sprinkle.

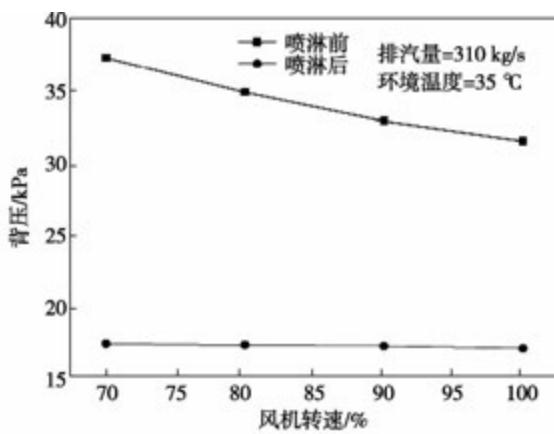


图 12 喷淋前后背压 - 风机转速关系

Fig. 12 The relationship between fan speeds and back-pressure before and after sprinkle

从图 14 中可以看出,当喷水量小于 G_{w1} 时,喷水量对直接空冷凝汽器的换热量影响最大。当喷水量大于 G_{w2} 时,喷水量的变化对换热量的影响很小。

从图 15 中可以看出,环境温度越高,喷水量的变化对背压影响的程度越大,当喷水量为 200 t/h 时,环境温度由 25 °C 变为 40 °C,背压下降分别为 4.01、4.70、5.63 和 5.91 kPa。在同一环境温度下,当喷水量小于 G_{w1} 时,增大喷水量对背压的影响比较大。继续增大水量,当喷水量大于 G_{w1} 小于 G_{w2} 时,喷水量对背压的影响稍小于前者,但增加喷水量

仍使背压持续下降。当喷水量大于 G_{w2} 时,继续增大喷水量,对背压的影响就很小了。综合上述分析,当环境温度较高时,喷水量变化对直接空冷凝汽器性能的影响比较大,且 G_{w2} 为最大蒸发喷水量。

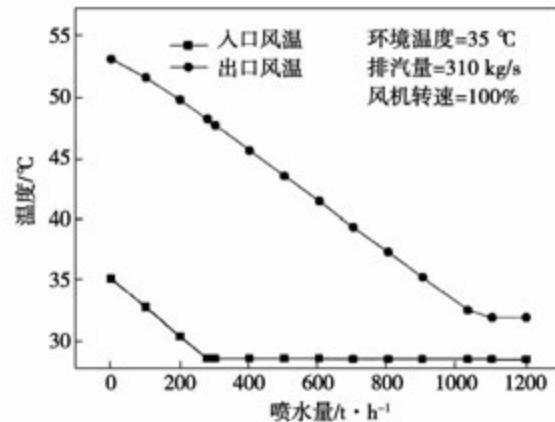


图 13 不同喷水量下换热前后空气的温度变化情况

Fig. 13 The change of the air temperature before and after converter under different water spray quantity

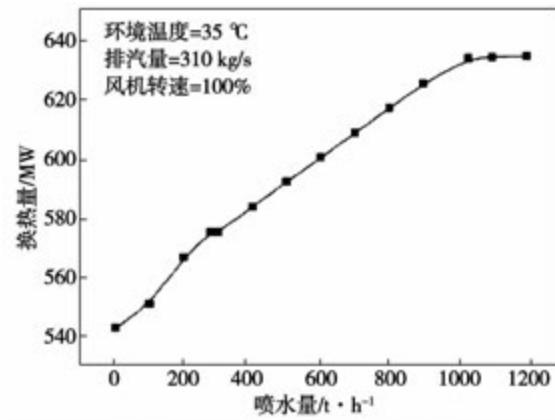


图 14 不同喷水量下换热量的变化情况

Fig. 14 The change of the heat transfer rate under different water spray quantity

从图 16 中可以看出,在不同排汽量下,排汽量较高时,喷水量的变化对背压影响比较大。当喷水量为 200 t/h 时,排汽量由 210 kg/s 变为 330 kg/s 时,背压变化分别为 4.91、5.38、5.52 和 5.75 kPa。在相同的排气量下,当喷水量小于等于 G_{w1} 时,相同喷水量下背压的降幅大于喷水量大于 G_{w1} 时背压的降幅。当喷水量大于 G_{w2} 时,继续增加喷水量,对背

压的影响就变得非常小。因此,在汽轮机高负荷运行时,采取喷淋措施效果更明显;同时,当喷水量大于 G_{w2} 时,继续增加喷水量,意义不大。从图17中可以看出,当风机转速较低时,喷水量的变化对背压的影响比较大。且当喷水量大于800 t/h时,在相同的喷水量下风机转速的变化对背压的影响很小。在相同的风机转速下,当喷水量小于 G_{w1} 时,喷水量的变化对背压的影响最大。当喷水量大于 G_{w2} 时,喷水量的变化对背压的影响非常小。

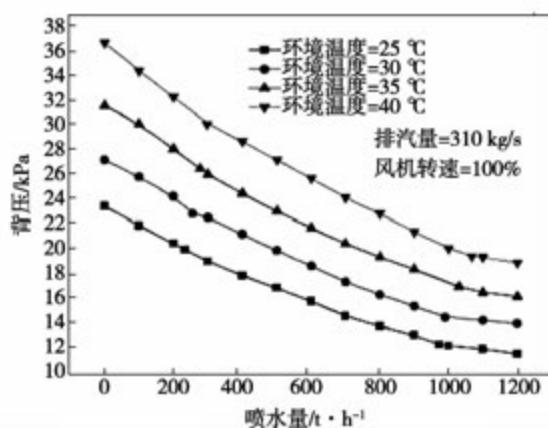


图 15 不同环境温度下背压 - 喷水量关系曲线

Fig. 15 The curve of back-pressure and water spray quantity under different ambient temperatures

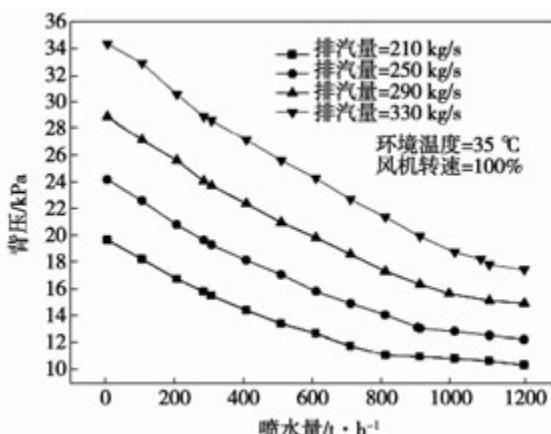


图 16 不同排汽量下背压 - 喷水量关系曲线

Fig. 16 The curve of the back-pressure and water spray quantity under different turbine exhaust steam flow rates

4 直接空冷凝汽器喷淋理论的应用与验证

为了验证喷淋性能计算模型的正确性,于2011年8月在某电厂对600 MW直接空冷机组分别针对不同负荷与环境温度等条件下进行了喷淋试验,并与理论计算进行了对比。相关试验结果如表1~表3所示。

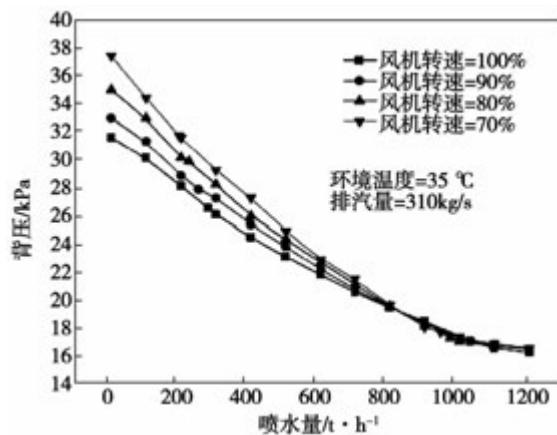


图 17 不同风机转速下背压 - 喷水量关系曲线

Fig. 17 The curve of back-pressure and water spray quantity under different fan speeds

表 1 机组 550 MW 负荷下喷淋结果

Tab. 1 The result of spraying in 550 MW unit load

机组负荷/MW	环境温度/°C	喷水量/t·h⁻¹	试验背压降低值/kPa	计算背压降低值/kPa
550	30.1	118.6	3.6	3.7
550	30	129.1	3.0	3.8
550	30	133.6	4.0	3.9
549	29.7	216.7	4.9	5.6
550	29.5	262.3	5.5	6.0

表 2 机组低负荷下喷淋结果

Tab. 2 The result of spraying in low load

机组负荷/MW	环境温度/°C	喷水量/t·h⁻¹	试验背压降低值/kPa	计算背压降低值/kPa
395	26.0	150	2.36	2.31
347	30.7	152	1.61	1.55
429	31	170	1.6	2.91
321	29.3	140	1.53	1.51
350	32.4	162	2.90	2.79

从表 1 与表 2 可以看出,不管是高负荷还是低负荷下,试验结果与理论计算结果得到的喷淋后背压变化趋势是一致的,并且两者的相对误差基本在 3%~5% 之间。除了针对不同负荷进行了喷淋试验外,也对不同环境温度也进行了喷淋试验。表 3 为机组负荷为 550 MW 左右,环境温度为 22 ℃左右时的试验结果。

表 3 机组 550 MW 负荷低温下喷淋效果

Tab. 3 The result of spraying under the low temperature in 550 MW unit load

机组负荷/MW	环境温度/℃	喷水量/t·h ⁻¹	试验背压降/kPa	计算背压降/kPa
523	22.45	138	2.39	1.81
517	21.41	180	2.89	2.9
536	22.23	138	2.97	2.58
561	23.61	100	1.47	1.51
520	22.29	138	1.91	1.91

通过比较表 1 和表 2 可以看出,高负荷比低负荷状态下,投运喷淋对应的背压平均多降约 2 kPa; 比较表 1 和表 3 发现,近似工况条件下,环境温度 30 ℃时投运喷淋水比 20 ℃时背压多降约 1.5 kPa。

5 结 论

以入口空气达到饱和状态和出口空气达到饱和状态为两个基准工况点,分析了喷水量变化时直接空冷机组运行背压的变化情况,并与喷淋试验进行了验证,得出结论:

(1) 通过建立喷淋换热模型,可以得到变工况下的喷水最大蒸发量,在此基础上继续增加喷水量,背压变化不明显。当喷水量小于喷水最大蒸发量时,增加喷水量,机组运行背压变化比较大,效果比较明显。

(2) 在相同的喷水量下,高负荷下投运喷淋水比低负荷平均多降约 2 kPa,在其它工况差不多的情

况下,环境温度为 30 ℃时投运喷淋水比环境温度为 20 ℃时背压多降约 1.5 kPa。

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(丛 敏 编辑)

uniformity of the radial temperature distribution at the outlet to get worsened, and to raise the inlet temperature can remarkably enhance the combustion efficiency, improve the uniformity of the radial temperature distribution at the outlet and raise the overall temperature. In addition, to increase the swirling number will make both combustion efficiency and overall temperature increase and the uniformity of the radial temperature distribution at the outlet become better accordingly. **Key Words:** swirling burner, turbulent flow combustion, number of steps, axial speed ratio, inlet temperature, swirling number

汽轮机排汽通道内湿蒸汽流动的数值研究 = **Numerical Study of the Wet Steam Flow in the Steam Exhaust Passage of a Steam Turbine** [刊, 汉] CAO Li-hua, ZHANG Hao-long (College of Energy Source and Power Engineering, Northeast University of Electric Power, Jilin, China, Post Code: 132012) , LIN Wen-bin (Electric Power Adjustment Experiment Limited Liability Co. , Fujian Pilot-scale Test Research Institute, Fuzhou, China, Post Code: 350007) , LIU Jia (Shandong Electric Power Engineering Consultancy Research Institute Co. Ltd. , Jinan, China, Post Code: 250013) //Journal of Engineering for Thermal Energy & Power. - 2015 ,30(3) . - 386 – 392

To analyze the flow conditions of the wet steam in the steam exhaust passage of a steam turbine, the software Fluent was used to conduct a numerical simulation of the flow inside the exhaust passage under various incoming flow conditions in combination with a phase-change model and a wet steam flow equation. It has been found that changes in the inlet steam wetness, swirling intensity and steam inlet angle will force the composition, location and intensity of the vortexes in the passage to produce changes. With an increase of the inlet steam wetness, the uniformity of the flow field at the outlet of the exhaust steam passage will enhance to a certain extent. With an increase of the inlet steam wetness, swirling flow intensity and steam inlet angle, the energy loss coefficient of the flow inside the exhaust steam passage will decline. **Key Words:** steam turbine, steam exhaust passage, wet steam, numerical analysis

直接空冷机组真空系统夏季喷淋性能研究 = **Study of the Summer Sprinkling Performance of a Vacuum System for Direct-air-cooled Units** [刊, 汉] ZHAO Hong-bin, XIE Pan, WU Hai-xia (College of Mechanical, Storage and Transportation Engineering, China University of Petroleum, Beijing, China, Post Code: 102249) //Journal of Engineering for Thermal Energy & Power. - 2015 ,30(3) . - 393 – 399

In recent years, the air-cooling technology for power plants has gained a rapid development, especially, the direct-air-cooling technology for power plants. The latter has become an important development tendency in the northwest

of China where is rich in coal but in a lack of water. Direct-air-cooled units will have a relatively high back pressure when operating in summer, seriously influencing the safe and economic operation of units and urgently needing to conduct a study and solve this problem. The authors conducted a theoretical analysis of the sprinkling effectiveness of a vacuum system in summer under off-design operating conditions and performed a verification of the model adopted through a sprinkling operation of the unit. In this process, the variation regularity of the back pressure under various sprinkling operating conditions was obtained and the maximum evaporation amount of water sprinkled was found out. When the amount of water sprinkled exceeds the maximum evaporation amount of water sprinkled, changes in the back pressure of the unit are relatively small. Under the condition that the amount of water sprinkled is constant, the back pressure decline effectiveness of the unit operating at a high load and a high temperature is more conspicuous than that at a low load and a low temperature. Therefore, to start up the sprinkling system when the unit is operating at a high load and a high temperature is relatively economic. The foregoing can offer theoretical guide for safe and economic operation of direct-air-cooled units in a high temperature atmosphere in summer. **Key Words:** direct-air-cooled, back pressure for operation, sprinkling in summer, amount of water sprinkled, performance analysis

Laval 喷管内湿蒸汽凝结流动的三维数值模拟 = **Three-dimensional Numerical Simulation of the Wet Steam Condensation Flow Inside a Laval Nozzle** [刊, 汉] SU Min-de, YU Jie-cheng, WEI De-qiang (College of Mechanical Engineering, Beijing Institute of Petrochemical Technology, Beijing, China, Post Code: 102617) //Journal of Engineering for Thermal Energy & Power. - 2015, 30(3). - 400 - 405

Based on the Wet-steam model in the software Fluent, a three-dimensional multi-operating-condition numerical simulation was performed of a transonic wet steam flow process accompanied with spontaneous condensation at a low pressure in a Laval nozzle and the influence of various temperatures and pressures at the inlet on such thermodynamic phenomena as spontaneous condensation, liquid droplet formation and condensation shock waves etc. and the liquid-phase parameters in the flow field was analyzed. It has been found that the higher the superheating degree at the inlet, the higher and greater the nucleation rate and the number of water droplets, however, the growth rate and average radius of water droplets will decrease with an increase of the superheating degree at the inlet. In the meantime, after the condensation emerges in the throat, there will exist an unsteady steam flow at the outlet, leading to a regular pulsation phenomenon. Hence, when a steam turbine is being in operation, one can decrease the number of water droplets precipitated and the average diameter of liquid droplets at the tail end of the outlet by lowering the