

抽汽加热暖风器系统机组能耗指标计算方法分析

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摘要: 本文介绍了机组在采用抽汽加热暖风器运行方式下能耗指标的计算方法。由于采用锅炉净效率 η_1 和燃料效率 η_2 两种不同的定义方法来计算锅炉效率,从而产生了不同的发电煤耗的计算方法。因为 $\eta_2 > \eta_1$,当将锅炉净效率 η_1 代入常规的发电煤耗计算公式时,机组发电煤耗偏高,放大了暖风器的不利影响,此时,依照本文介绍的修正公式可对计算结果进行修正;而当使用锅炉燃料效率 η_2 计算机组发电煤耗时则不需要进行修正。因此,本文建议机组考核试验采用锅炉燃料效率作为试验数据处理的基准数据。

关键词: 燃料效率; 净效率; 发电煤耗; 热平衡

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引言

暖风器系统是目前国内外普遍采用的用来提高空气预热器入口的冷风温度,防止空气预热器发生低温腐蚀及堵灰现象的设备。暖风器的加热热源可以是汽轮机抽汽、电加热器或其它形式的热源。对于汽轮机抽汽加热暖风器系统而言,其对整个循环系统的影响主要表现在:(1)空气预热器入口冷风温度增加将使锅炉排烟温度升高,锅炉排出系统的能量损失增加;(2)汽轮机抽汽量增加,使进入冷凝器的排汽量减少,冷端损失减少;(3)汽轮机抽汽加热暖风器后不再参与做功,相同进汽流量下,汽轮机的输出功率减少。上述三方面影响中,排烟温度升高及输出功率减少对系统的经济性产生不利的影 响;而冷端损失减少则对系统经济性产生有利的影响。综合考虑三方面的影响及理论计算表明:暖风器投运会使机组经济性下降,且暖风器出口冷空气温度越高,机组的经济性下降越显著^[1-2]。

针对暖风器系统投运对机组运行经济性的影响,西北电力设计院张建中等学者和西安交通大学

林万超教授均进行了详细的理论分析与公式推导^[1-2];此外,李笑乐等多位学者论述了暖风器对锅炉效率的影响,根据其研究结果,暖风器投运后将使锅炉效率降低^[3-8];但近期也有学者提出不同看法,王金旺等通过计算表明暖风器投运后锅炉效率将升高^[9]。

由于汽轮机抽汽加热暖风器系统对锅炉和汽轮机均产生影响,单纯从锅炉效率或汽轮机热耗率的角度来分析其对经济性的影响均不够全面,需结合锅炉和汽轮机两方面共同考虑。

本文以热力学第一定律为基础,综合考虑暖风器对锅炉和汽轮机的影响,分析了暖风器对机组经济性影响的计算方法。

1 暖风器对机组经济性影响计算方法

1.1 锅炉效率计算方法

锅炉效率是指以锅炉热平衡为基础,锅炉有效输出热量与输入热量的比值。但现行多种标准对锅炉效率的定义存在一定的差异性。国内、外普遍采用的锅炉热效率计算标准包括《火力发电厂技术经济指标计算方法》(DL/T904-2004)、《电站锅炉性能试验规程》(GB/T 10184-1988)和《Fired Steam Generators Performance Test Code》(ASMEPTC4-1998)^[10-13]。其中,GB/T10184-1988标准中锅炉效率的定义为锅炉输出热量与进入锅炉系统的总热量之比,进入锅炉系统的总热量指燃料输入热量和外来热量或由其它热源加入到系统的热量之和;DL/T904-2004标准中锅炉效率的定义为锅炉输出热量与进入锅炉系统的燃料热量之比;ASMEPTC4-1998(包括其中文译本)标准中对上述

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两种锅炉效率均有定义,分别为净效率和燃料效率,该标准中通常使用燃料效率及燃料高位发热量作为计算基准。

锅炉热平衡方程如式(1)所示,式中计算的边界温度取为暖风器入口空气温度,即暖风器在锅炉计算边界内,其输入热量以外来热量处理。在此基础上可得到锅炉净效率 η_1 和燃料效率公式 η_2 的计算方法分别为式(2)和式(3)。

$$B \times Q_{ar,net} + Q_{wr} = Q_o + Q_L \quad (1)$$

$$\eta_1 = \frac{Q_o}{B \times Q_{ar,net} + Q_{wr}} = 1 - \frac{Q_L}{B \times Q_{ar,net} + Q_{wr}} \quad (2)$$

$$\eta_2 = \frac{Q_o}{B \times Q_{ar,net}} = 1 - \frac{Q_L}{B \times Q_{ar,net}} + \frac{Q_{wr}}{B \times Q_{ar,net}} \quad (3)$$

式中: B —燃料消耗量,kg/s; $Q_{ar,net}$ —燃料低位发热量,kJ/kg; Q_{wr} —外部热源带入的热量,kW; Q_o —锅炉有效输出热量,kW; Q_L —锅炉损失热量,kW,通常有 $\eta_2 \geq \eta_1$ 。

当将燃烧输入热量折算到标准煤消耗量 B_1 时有:

$$B_1 = \frac{B \times Q_{ar,net}}{29\,308} \quad (4)$$

1.2 汽轮机热耗率计算方法

汽轮机热耗率是衡量汽轮机工作性能的关键参数,热耗率是指汽轮机组每生产1 kWh电能所消耗的热量,其计算方法如式(5)所示。

$$q = \frac{Q_{sr}}{P_e} \quad (5)$$

式中: q —汽轮机热耗率(非供热机组),kJ/kWh; P_e —发电机出线端电功率,kW; Q_{sr} —由外部热源获得的热量,kW,其计算方法如式(6)所示。

$$Q_{sr} = (D_{zq} \times h_{zq} - D_{gs} \times h_{gs} + D_{zr} \times h_{zr} - D_{lzt} \times h_{lzt} - D_{gj} \times h_{gj} - D_{zj} \times h_{zj} + \sum_{i=1}^m D_{go_i} \times h_{go_i}) \quad (6)$$

式中: D —工质流量,kg/s; h —工质焓值,kJ/kg,下标的意义分别为: zq —主蒸汽; gs —给水; zr —再热蒸汽; lzt —冷再热蒸汽; gj —过热器减温水; zj —再热器减温水; go_i —锅炉侧排出或漏出的第 i 股蒸汽或水。锅炉输出的有效热量 Q_o 在进入汽轮机边界前有会一定的损失,即管道损失,可定义管道效率 η_{gd} 予以考虑,因此有:

$$Q_{sr} = Q_o \times \eta_{gd} \quad (7)$$

当机组抽取一部分蒸汽作为暖风器加热热源时,汽轮机由锅炉侧吸收的总热量保持不变,但加热暖风器的这部分蒸汽不参与做功,汽轮机输出功率 P_e 减少,这相当于增加了汽轮机的热耗率。汽轮机输出功率的变化可由式(8)进行计算:

$$\Delta P_e = Q_{nf} \times \eta_i \quad (8)$$

式中: Q_{nf} —暖风器热功率,kW; η_i —暖风器热源辅助蒸汽对应的抽汽效率。

汽轮机热耗率由汽轮机性能试验结果确定,其中已包含暖风器用蒸汽的影响。

1.3 发电煤耗率的计算方法

机组的发电煤耗和供电煤耗是衡量机组经济性的重要指标,发电煤耗 b 是指火力发电厂每生产或供应1 kWh电能所消耗的燃料量,通常用g/kWh来表示,可由式(9)计算。

$$b = \frac{1\,000 \times B}{P_e} \quad (9)$$

在一段统计时间内要直接测量燃料消耗量和输出功率较难实现,为较为准确的评估机组的能耗指标,通常使用锅炉效率和汽轮机热耗率等参数进行反平衡计算。当暖风器投入运行后,锅炉净效率和燃料效率的定义存在一定的差异性,机组能耗指标的计算也将发生变化。

基于锅炉净效率的定义时,根据式(2)可得到机组燃料消耗量的表达式(10)为:

$$B = \frac{Q_o}{\eta_1 \times Q_{ar,net}} - \frac{Q_{nf}}{Q_{ar,net}} \quad (10)$$

基于锅炉燃料效率的定义时,根据式(3)可得到机组燃料消耗量的表达式(11)为:

$$B = \frac{Q_o}{\eta_2 \times Q_{ar,net}} \quad (11)$$

式(10)中仅考虑暖风器的热量为外热源带入的热量,即 $Q_{nf} = Q_{wr}$ 。式(10)和式(11)中 η_1 、 η_2 、 Q_{nf} 和 $Q_{ar,net}$ 均可以通过试验得到,而 Q_o 作为锅炉与汽轮机之间传递的有效能量,起关键连接作用。由式(5)可得汽机输出功率 P_e 的表达式(12)为:

$$P_e = \frac{Q_{sr}}{q} \quad (12)$$

式(12)中的汽轮机热耗率 q 可通过试验测量, Q_{sr} 与 Q_o 成比例,如式(7)所示。分别将式(10)、式(11)与式(7)和式(12)带入式(9)可得基于燃料效率的供电煤耗计算式(13)为:

$$\begin{aligned}
 b &= 1\,000 \times \frac{q}{\eta_{\text{gd}} \times \eta_2 \times Q_{\text{ar,net}}} \\
 &= 1\,000 \times \left(\frac{q}{\eta_{\text{gd}} \times \eta_1 \times Q_{\text{ar,net}}} - \frac{Q_{\text{nf}}}{Q_{\text{ar,net}} \times P_e} \right) \quad (13)
 \end{aligned}$$

式(13)所列即为汽轮机抽汽加热暖风器系统采用不同锅炉热效率计算方法时,机组发电煤耗率的计算公式。需要注意的是,整个计算过程基于相同的锅炉和汽轮机性能试验结果,只是在数据处理方法上存在一定的差异。

式(13)中数据按标准煤发热量进行折算后即可得到机组发电标准煤耗率的值。

1.4 计算方法分析

通常用式(13)中等式中间的公式作为机组发电煤耗计算的反平衡公式,即式(14)。当无外部热量加入系统时,即 $Q_{\text{wr}} = Q_{\text{nf}} = 0$,此时锅炉效率 $\eta_g = \eta_2 = \eta_1$,即采用燃料效率与净效率定义计算得到的机组发电煤耗数值相等。

$$b = 1\,000 \times \frac{q}{\eta_{\text{gd}} \times \eta_g \times Q_{\text{ar,net}}} \quad (14)$$

当采用汽轮机抽汽加热暖风器时,由于 $\eta_2 > \eta_1$,此时如果仍按照式(14)进行计算,则按净效率 η_1 (式中 η_g)计算得到的发电煤耗值要高于按燃料效率 η_2 (式中 η_g)的计算结果,其原因在于净效率的计算方法反映的是锅炉有效输出热量与总输入热量的比值,相当于把暖风器的热量折算成一部分燃料的热量,因此,发电煤耗计算值增大。此时,按式(13)中等式最右边括号内最后一项修正后(修正项为负值),可将暖风器的影响扣除,机组发电煤耗降低,从而与按燃料效率 η_2 的计算结果一致。

综上所述,当对采用汽轮机抽汽加热暖风器系统的经济性进行评估或性能考核试验时,采用燃料效率计算方法结合汽轮机性能试验数据进行计算时,即按式(14)进行计算,公式简单,意义明确。当采用净效率定义计算锅炉效率时必须对发电煤耗结果进行修正,按式(13)进行,否则将使暖风器的负面影响放大,不能准确反映机组的能耗水平。

2 结 论

本文基于热力学第一定律介绍了汽轮机抽汽加

热暖风器系统运行工况下机组发电煤耗的计算公式。根据本文的分析结果可得到如下结论:

(1) 对于汽轮机抽汽加热暖风器系统而言,基于净效率 η_1 和燃料效率 η_2 定义下,锅炉效率的计算方法不同,且有 $\eta_2 > \eta_1$;

(2) 暖风器投运后造成机组输出功率的减少应以汽轮机性能试验结果为准,表现为汽轮机热耗率增加,功率减少量也可由暖风器热功率与相应抽汽级抽汽效率进行估算;

(3) 采用燃料效率的定义计算锅炉效率时,可直接按式(14)计算机组的发电煤耗,计算公式简单,意义明确;

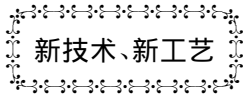
(4) 采用净效率的定义计算锅炉效率时,应在式(14)的计算结果上对发电煤耗进行修正,修正方法按本文式(13)中等式右边最后一项进行;

(5) 按两种锅炉效率的定义方法均可对机组的发电煤耗进行准确的计算,但由于燃料效率的定义明确、公式简单,推荐采用此种方法作为汽轮机抽汽加热暖风器系统的能耗评估计算方法。

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- (单丽华 编辑)



GE - Alstom 联合企业带来 Uberturbine 的梦想

据《Gas Turbine World》2014 年 7 ~ 8 月刊报道 ,1995 年推出的 GEMS9001H 燃气轮机第一级动叶进口温度为 1 426 ℃。四级涡轮的第 1、2 级为蒸汽冷却 ,包括第 1、2 级涡轮的静叶和动叶及第 1 级涡轮机匣。

由于采用蒸汽冷却 ,H 型燃机比空气冷却的 G 型燃机联合循环的功率增加 60 MW(从 420 MW 增加到 480 MW) ,效率提高 2%(从 58% 增加到 60%) ,NO_x 排放减少一半。

Alstom 公司于 1994 年推出的新型高效的 GT24 和 GT26 型燃气轮机采用了 SCS(顺序燃烧系统) 2 个环形燃烧室由第一级涡轮叶轮隔开。2/3 的燃料在上游燃烧室中与空气预混并点火燃烧 ,驱动第一级涡轮; 剩余 1/3 燃料在第 2 个燃烧室中与空气预混点火燃烧 ,联合的热燃气驱动后面的 4 级涡轮。

并未追求过高的涡轮进口温度 ,通过使用顺序燃烧 GT24 和 GT26 燃气轮机就取得了很高的效率和比功 ,简单循环效率高达 40%(41%) ,联合循环效率达到 58.4%(59.5%) 。

现在 ,GE - Alstom 打算使 GE 的蒸汽冷却涡轮技术和 Alstom 的顺序燃烧设计相结合 ,以便研制出能够达到 64% 或 65% 联合循环净效率和实用的蒸汽冷却顺序燃烧的燃气轮机。

报导还阐述了该循环详细的理论和实用分析及其设计限制。

(吉桂明 摘译)

Detailed analysis indicates that the specific heat load of the boiler body , steam water system and hot air system of the boiler system are relatively small , and the heat loss is proportional to the area. But the heat dissipation of the heat insulating separator and the return system is 5 times the former , with 16.2% of the area generating 47.6% of the heat dissipation. Therefore , there is a large degree of system uncertainty on the method of estimating the heat loss of circulating fluidized bed boiler outlined by the current national standard and industry standard. **Key words:** circulating fluidized bed , heat loss , specific heat load , uncertainty analysis

使用不同燃烧器对火筒式加热炉的影响分析 = **Effect of Different Burner on The Behaviors of Drum Type Heating Furnace** [刊 , 汉] HAN Shou-peng (University of Shanghai for Science and Technology , Shanghai , China , Post Code: 200093) , LIAO Xiao-wei , LI Ya-zhou (China Special Equipment Inspection and Research Institute , Beijing 100013) , XU Hong-tao (University of Shanghai for Science and Technology , Shanghai , China , Post Code: 200093) // Journal of Engineering for Thermal Energy & Power. -2016 , 31(10) . -43 ~ 49

This paper adopts experimental and numerical methods to analyze the influence of two different burners on the temperature field , flow field and nitrogen oxide generated during the process of combustion in drum type heating furnace. The input power of two burners is both set to be 700 KW and some conclusions are drawn as follows: The average temperature in the furnace generated by the forced air blast burner is higher than that by the atmospheric burner. The flame deflection by the atmospheric burner is worse than that by the forced air blast burner. The top of furnace is easy to be washed by the gas to generate a high-temperature region when the atmospheric burner is used. The gas flow at the bottom of the furnace is lower , and the heat transfer condition is poor. The contents of NO_x in the flue gas from the combustion in the atmospheric burner and forced air blast burner are 0.01464% and 0.01512% , respectively. **Key words:** burner , heating furnace , numerical simulation

抽汽加热暖风器系统机组能耗指标计算方法分析 = **Calculation of Coal Consumption Rate for Power Plant with Steam Turbine Extractions Heating Air Heater System** [刊 , 汉] DING Xing-wu (Huaneng Shandong Power Generation Co. , Ltd. Jinan , Shandong , Post Code: 250002) , FAN Qing-wei (Xi'an Thermal Power Research Institute Co. , Ltd. Xi'an , Shaanxi , China , Post Code: 710032) , SU Yong-ning (Huaneng Laiwu Power Generation Co. , Ltd. Laiwu , Shandong , China , Post Code: 251100) , XIE Tian (Xi'an Thermal Power Research Institute Co. , Ltd. Xi'an , Shaanxi , China , Post Code: 710032) // Journal of Engineering for Thermal Energy & Power. -2016 , 31(10) . -50 ~ 53

In this paper , two different calculation methods for coal consumption rate of power plant with steam turbine extractions heating the air heater system are introduced in detail. By taking the turbine heat consumption rate together with the boiler's net efficiency η_1 and fuel efficiency η_2 respectively to the common formula for calculating the coal consumption rate , the results are different. Using the boiler's net efficiency yields higher coal consumption rate due to $\eta_2 > \eta_1$. In this case , a correction formula to consider the air heater's energy that affects the fuel consumption is necessary to obtain the correct result. When using the boiler's fuel efficiency to calculate the coal consumption rate , there is no need to correct the result. Therefore , we suggest using the boiler's fuel efficiency to calculate the coal

consumption rate. **Key words:** fuel efficiency μ net efficiency μ coal consumption rate μ heat balance

中小型火电机组凝汽余热利用供热系统集成研究 = **Configuration Research on Waste Heat Utilization System of Condensing Steam for Middle and Small-sized Thermal Power Unit** [刊, 汉] LI Yan, MA Yi-feng, ZHANG Yong-gui (College of Civil Engineering & Mechanics, Yanshan University, Qinhuangdao, China, Post Code: 066004), FU Lin (School of Architecture, Tsinghua University, Beijing, China, Post Code: 100083) // Journal of Engineering for Thermal Energy & Power. -2016, 31(10). -54~58

There is tremendous energy saving potential in the waste heat recovery of condensing steam for middle and small-sized thermal power unit. Aiming at middle and small-sized water-cooled unit, this paper combines the low-vacuum operation and the absorption heat pump technologies, and then puts forward a new system of condensing steam waste heat utilization. This system overcomes the high investment and the large-scale occupation of the absorption heat pump, and therefore increases the feasibility to recover the waste heat of condensing steam. Taking the 135 MW water-cooled unit as research object, for the ratio of the extraction and the exhausted stem of the turbine, and its back pressure, we set the security constraints, through the safety analysis on the last-stage blade of the steam turbine. Also, the system is optimized through analyzing its energy efficiency and economy. Results above can be used to guide the design of condensing steam waste heat utilization system for middle and small-sized thermal power unit. **Key words:** turbine unit, waste heat recovery of condensing steam, system optimization

双螺杆膨胀机的发电特性试验研究 = **Experimental Study on Electricity Output Characteristics of Process Gas Twin Screw Expander** [刊, 汉] XU Ming-zhao, YANG Xiao-qiang, DIAO Anna, YANG Yi (Shanghai Marine Diesel Engine Research Institute, Shanghai 200072) // Journal of Engineering for Thermal Energy & Power. -2016, 31(10). -59~62

The problem of using the screw expander to replace the industry pressure and temperature reducing device was theoretically analyzed and experimentally investigated. Thermodynamic model of the under-expansion working process in twin-screw expander was proposed in this paper. Through the analysis of the theoretical and experimental data, the results indicate that under-expansion can lead to the reduction in electrical generation, and the losses increases with the suction pressure. Due to the influence of heat exchange and leakage, the actual expansion process is close to isothermal expansion. The theoretical calculation results agree reasonably well with the experimental data when the suction pressure is up to 0.238 MPa, and the maximum and minimum deviations are 18% and 10%, respectively. **Key words:** pressure and temperature reduction, twin-screw expander, under-expansion

不同堆放条件下煤堆压实最低不适用风速研究 = **Study on the Minimum Inapplicable Wind Velocity of Coal Stockpile Compaction under Different Conditions of Stacking** [刊, 汉] DONG Zi-Wen, WU Xian, QI Qing-Jie, ZHENG Dan (College of Safety Science and Engineering, Liaoning Technical University, Fuxin Liaoning, China, Post Code: 123000) // Journal of Engineering for Thermal Energy & Power. -2016, 31(10). -63~71